

# Raschig Super-Ring® Plus

## Product Bulletin 251

The design of Raschig Super-Ring® was published in 1998 and had set new standards in the performance of random packings.

Nowadays it is called the first fourth generation random packing compared to earlier designs like Raschig-Rings, Pall-Rings and third generation packings. Soon after the Raschig Super-Ring® was available to the Industry it was a new reference line for packing comparisons in terms of pressure drop, capacity and efficiency.



**FRI and SRP tested**

**A new Random Packing offers  
new advantages in performance**



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# Raschig Super-Ring® Plus

Raschig Super-Ring® Plus is the result of a consequent design development based on many years of research. The target was to stay with all advantages of Raschig Super-Ring® but improve capacity and reduce pressure drop.



The preferred principles of gas/liquid countercurrent flow, coming along with Raschig Super-Ring® Plus are as follows:

- **Minimize pressure drop** by arranging flat sinusoidal strips to an extreme open structure
- **Maximize capacity** by film flow preference on continuous sinusoidal strip arrangements
- **Maximize efficiency** by minimizing droplet formation inside the packing
- **Minimize foaming tendency** by minimizing droplet development and low pressure drop
- **Minimize fouling sensitivity** by generating continuous liquid films wetting the entire packing element
- **Maximize the effective surface area** by spreading the liquid film all over the packing
- **Maximize the open column cross section area** by optimized packing orientation
- **Increase mechanical strength** by strip rotation





# Raschig Super-Ring<sup>®</sup> Plus

Technical data of the Raschig Super-Ring<sup>®</sup> Plus

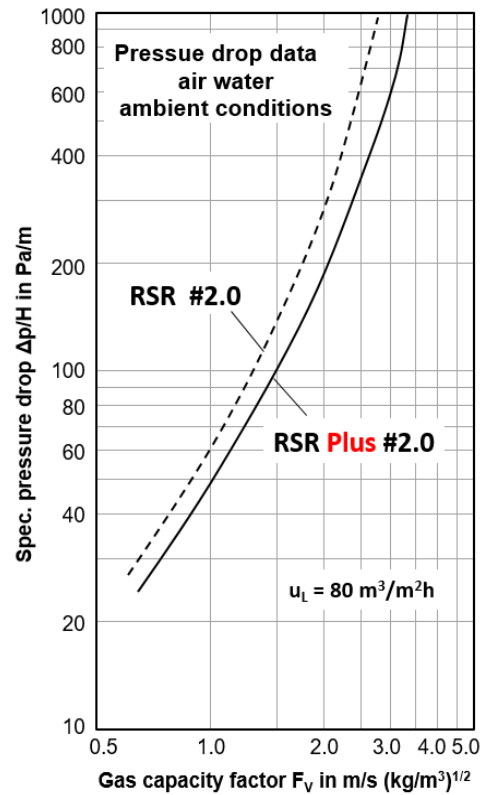
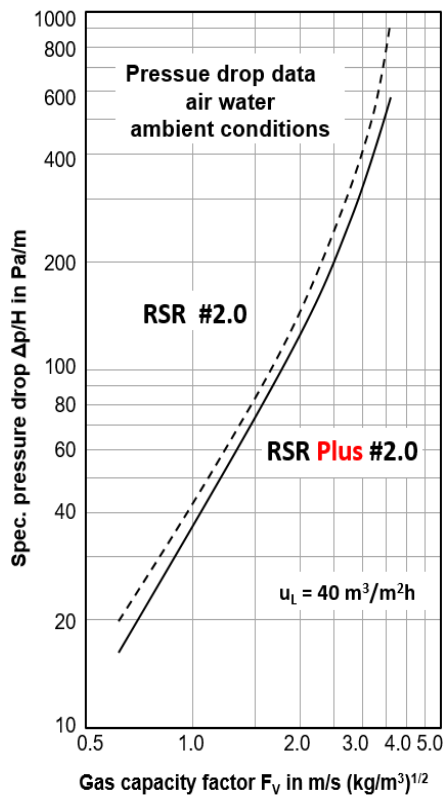
Size	Material	Surface area m <sup>2</sup> /m <sup>3</sup>	Free Volume %
0.7	Metal	175	98
1	Metal	150	98
2	Metal	100	98





# Raschig Super-Ring<sup>®</sup> Plus #2

The following figures demonstrate the pressure drop advantage of Raschig Super-Ring<sup>®</sup> Plus #2 compared to Raschig Super-Ring<sup>®</sup> #2.



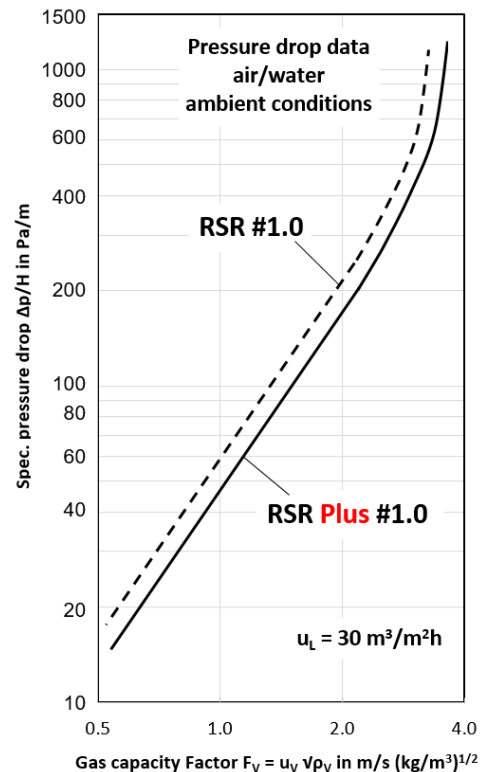
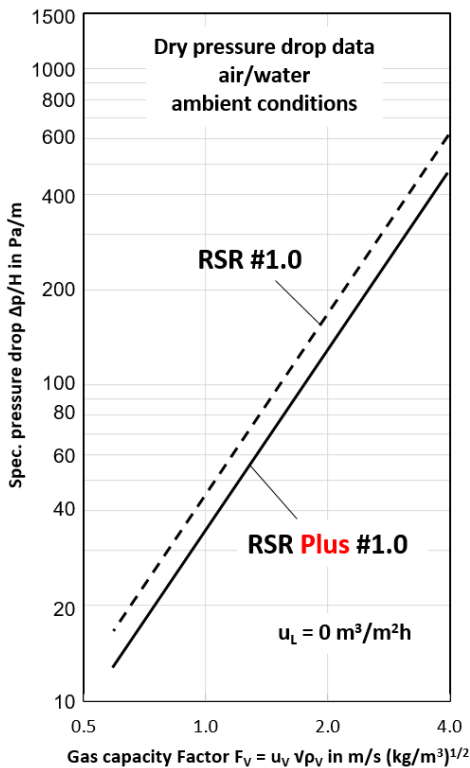
In the air/water simulator the pressure drop and capacity advantage of Raschig Super-Ring<sup>®</sup> Plus #2 became obvious. The packing opens up the column cross section area by its special design which results in noticeable fluiddynamic benefits. A **capacity advantage of 8 %** and **pressure drop reduction of 10 %** was measured.





# Raschig Super-Ring<sup>®</sup> Plus #1

The following figures demonstrate the pressure drop advantage of Raschig Super-Ring<sup>®</sup> Plus #1 compared to Raschig Super-Ring<sup>®</sup> #1.



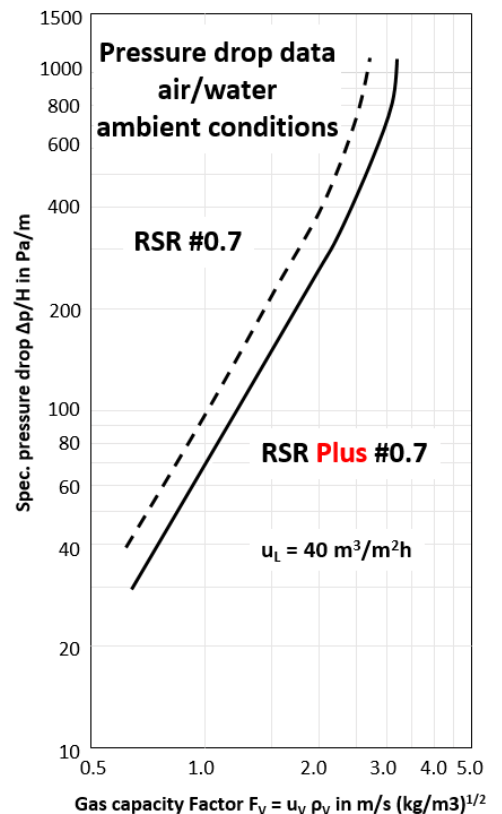
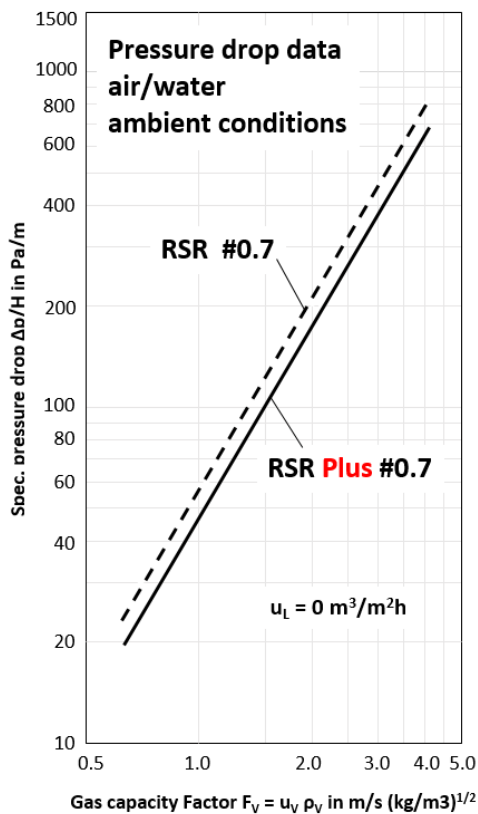
In the air/water simulator the pressure drop and capacity advantage is also proved for Raschig Super-Ring<sup>®</sup> Plus #1. A capacity advantage of 8 % and pressure drop reduction of 10 % was measured.





# Raschig Super-Ring® Plus #0.7

The following figures demonstrate the pressure drop advantage of Raschig Super-Ring® Plus #0.7 compared to Raschig Super-Ring® #0.7.



In the air/water simulator the pressure drop and capacity advantage is also proved for Raschig Super-Ring® Plus #0.7. A capacity advantage of 8 % and pressure drop reduction of min. 10 % was measured.

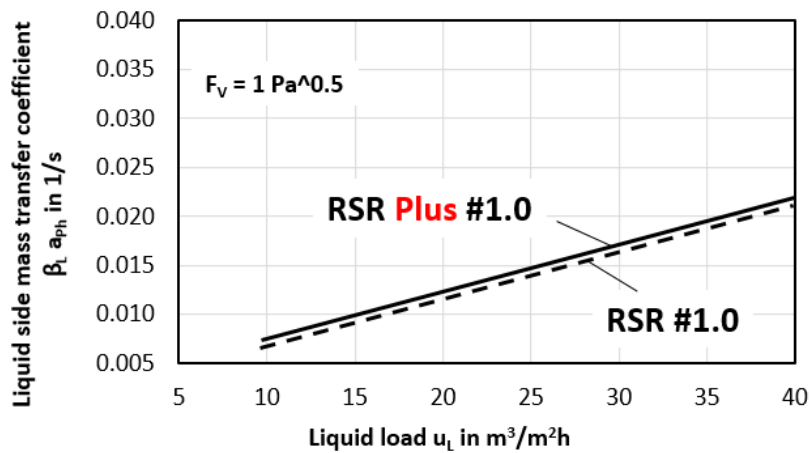




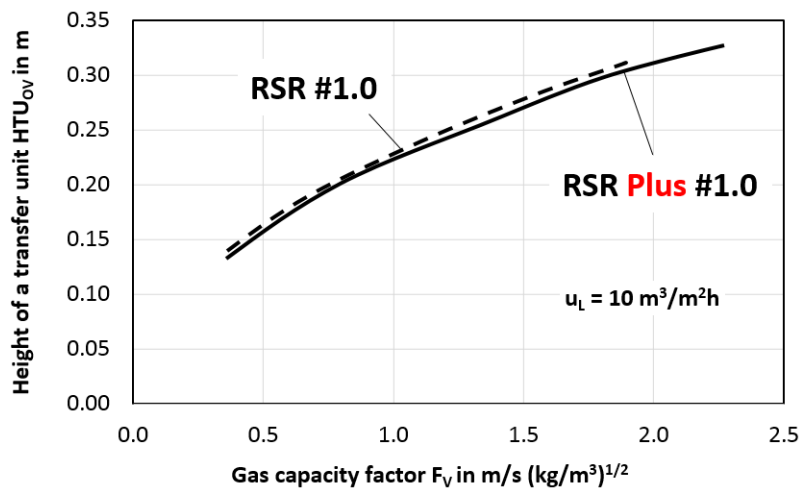
# Raschig Super-Ring<sup>®</sup> Plus #1

## Mass transfer efficiency of metal

Desorption of CO<sub>2</sub> from water into an atmospheric air stream



Absorption of NH<sub>3</sub> from air in water in the gaseous phase



The efficiency of Raschig Super-Ring<sup>®</sup> Plus #1 is practically the same as Raschig Super-Ring<sup>®</sup> #1

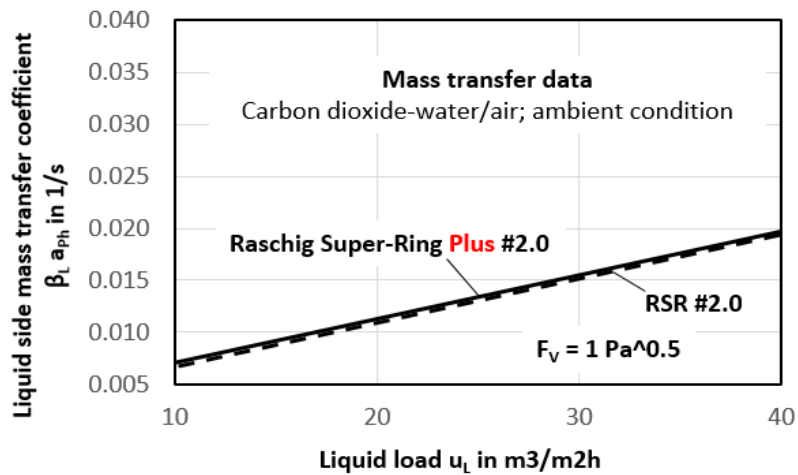




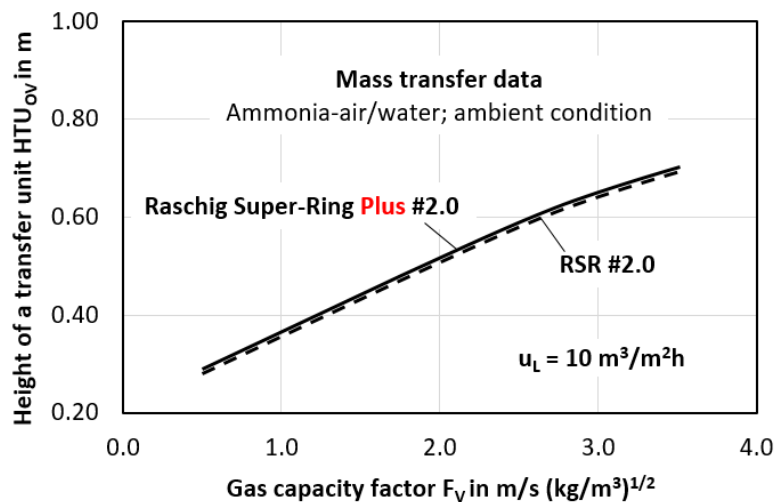
# Raschig Super-Ring® Plus #2

## Mass transfer efficiency of metal

Desorption of CO<sub>2</sub> from water into an atmospheric air stream



Absorption of NH<sub>3</sub> from air in water in the gaseous phase



The efficiency of Raschig Super-Ring® Plus #2 is practically the same as Raschig Super-Ring® #2







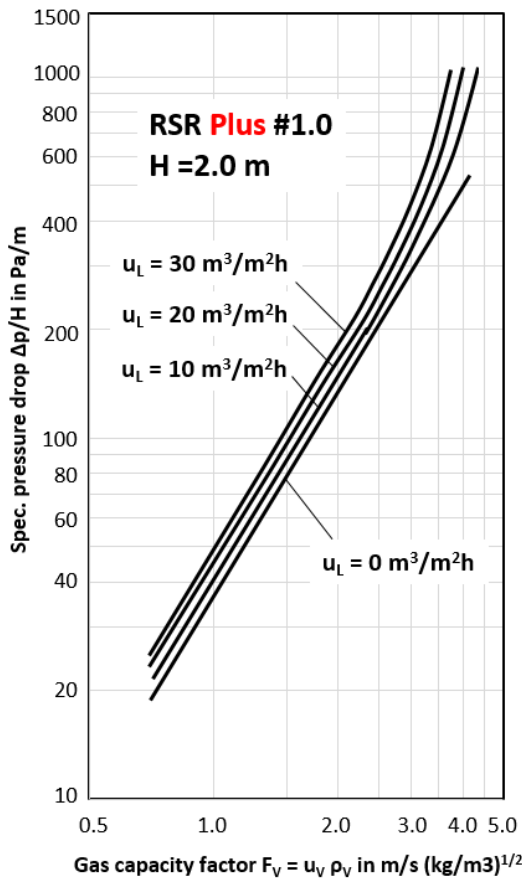
# Raschig Super-Ring® Plus

## Pressure Drop data

system: air/water

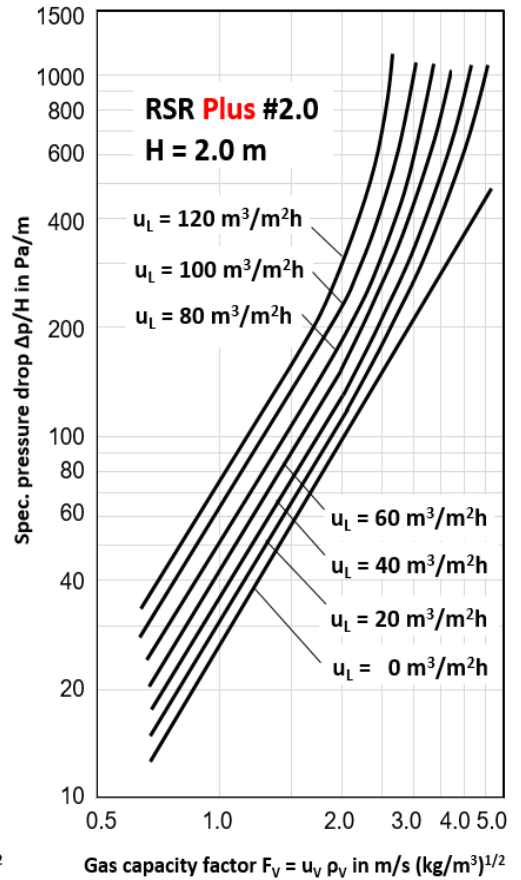
### Raschig Super-Ring® Plus #1

Column diameter: 0.288 m



### Raschig Super-Ring® Plus #2

Column diameter: 0.450 m





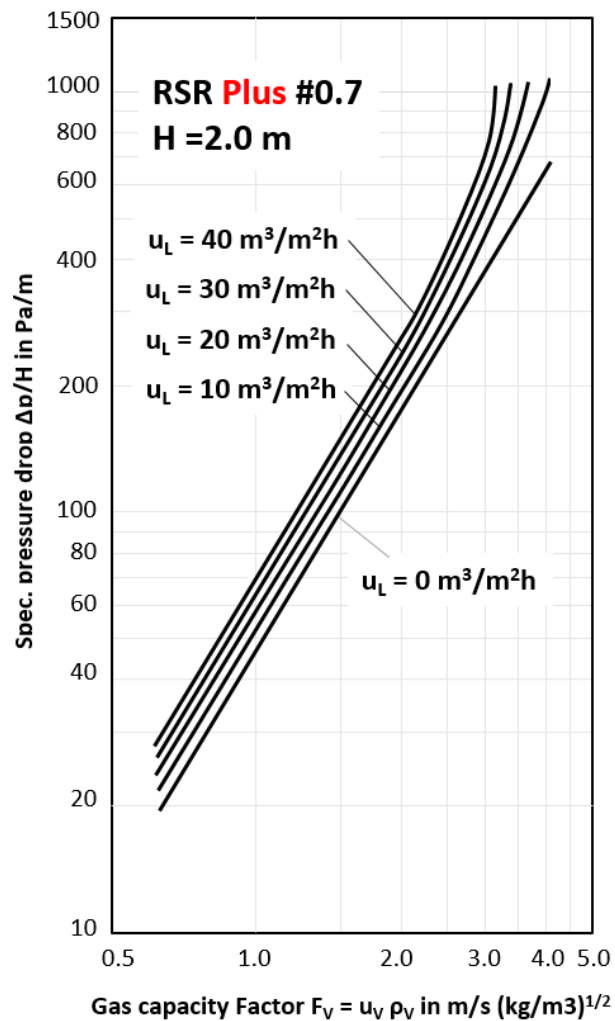
# Raschig Super-Ring<sup>®</sup> Plus

## Pressure Drop data

system: air/water

Raschig Super-Ring<sup>®</sup> Plus #0.7

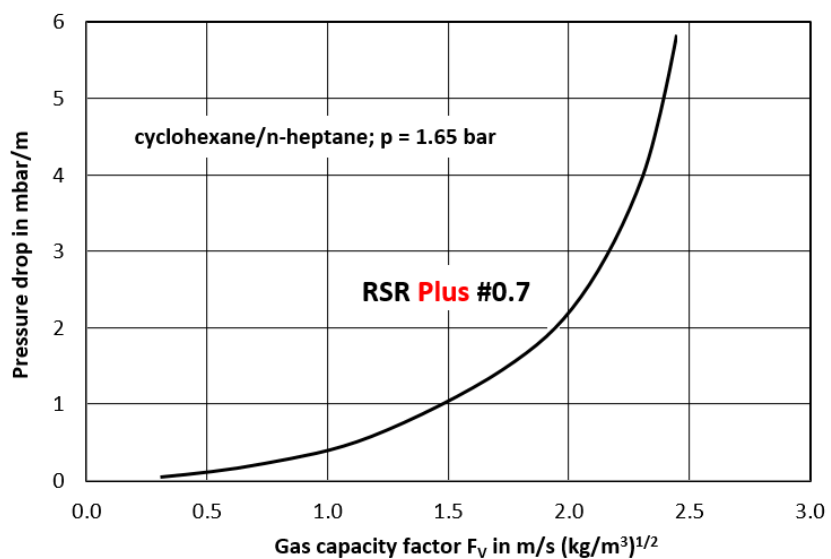
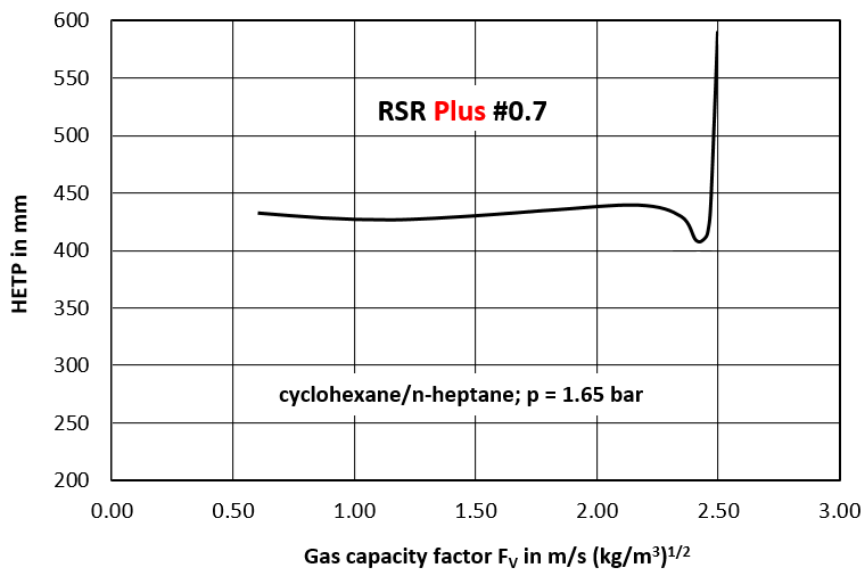
Column diameter: 0.288 m





# Raschig Super-Ring® Plus #0.7 SRP tested

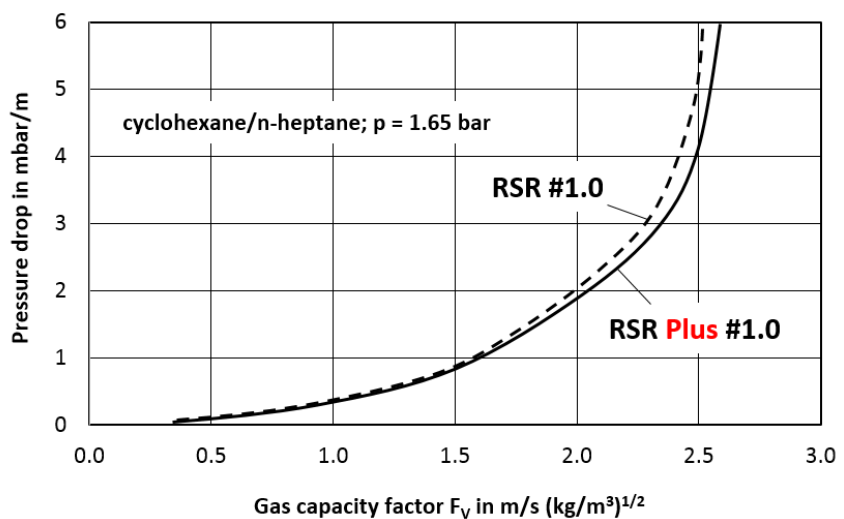
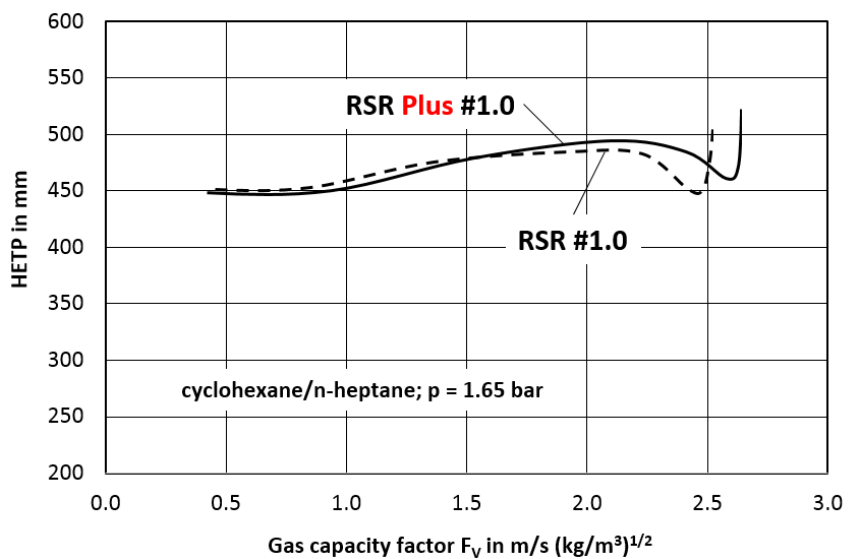
Height equivalent to a theoretical plate HETP  
and pressure drop per meter of packing  
height for metal under distillation test conditions





# Raschig Super-Ring<sup>®</sup> Plus #1 SRP tested

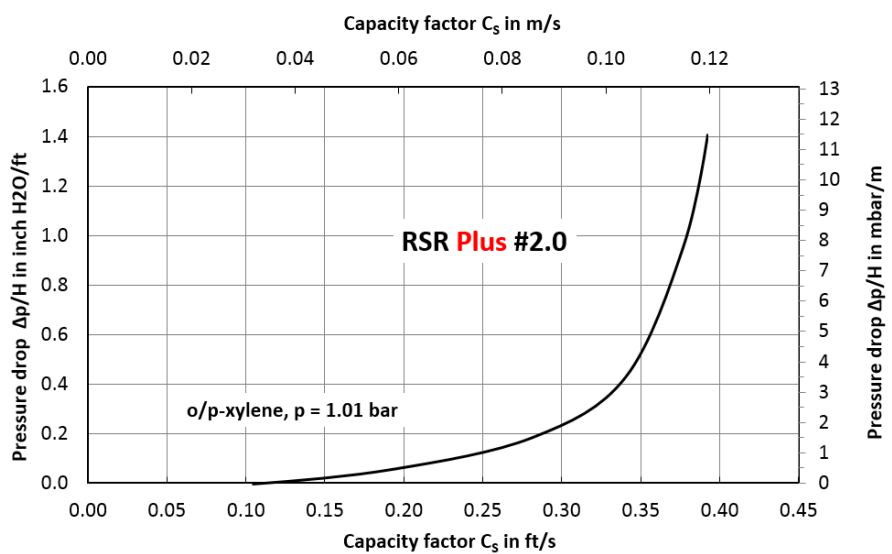
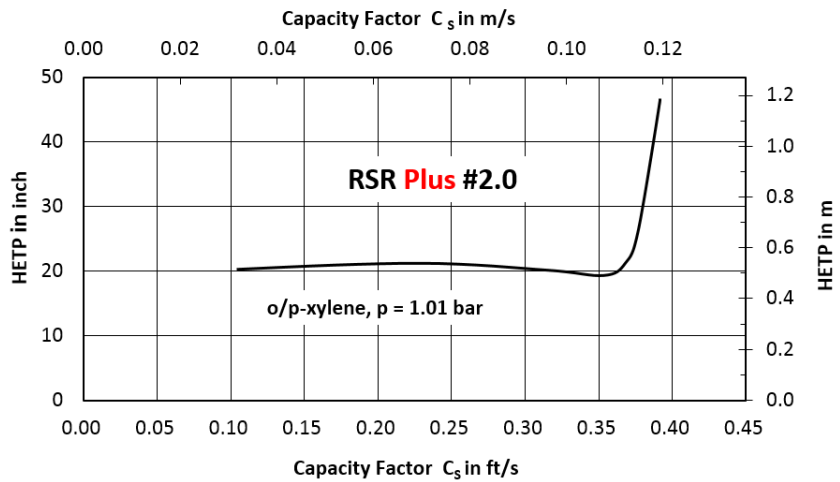
Height equivalent to a theoretical plate HETP  
and pressure drop per meter of packing  
height for metal under distillation test conditions





# Raschig Super-Ring<sup>®</sup> Plus #2 FRI tested

Height equivalent to a theoretical plate HETP  
and pressure drop per meter of packing  
height for metal under distillation test conditions



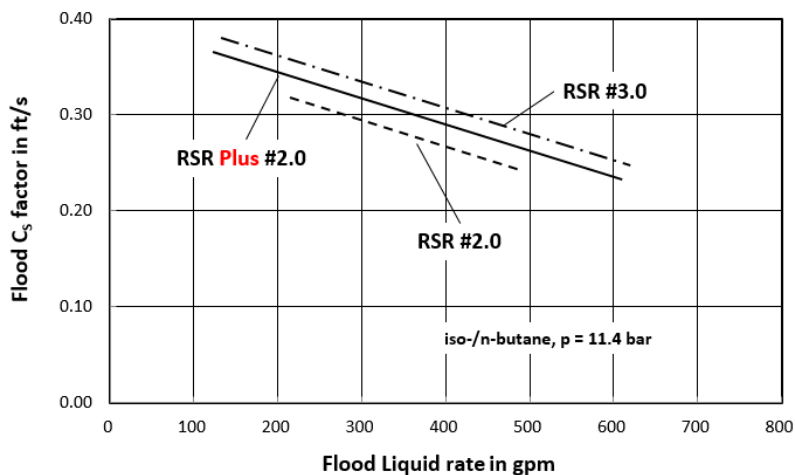
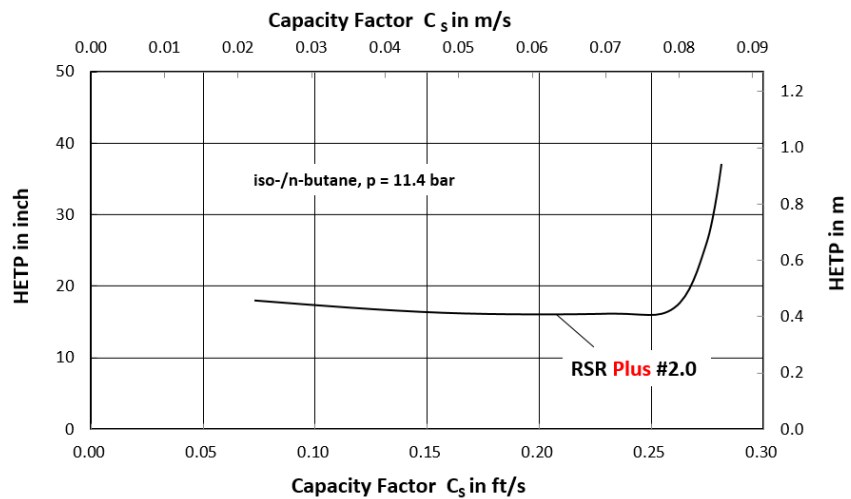


# Raschig Super-Ring<sup>®</sup> Plus #2

Height equivalent to a theoretical plate HETP  
and flooding curve of packing  
for metal under distillation test conditions

### Efficiency Comparison

FRI HP test column D = 1.22 m = 4 ft; system: Iso-butane/N-butane, p = 11.4 bar = 165 psia



# Nomenclature

## Latin symbols

$a$	$m^2/m^3$	specific surface area of packing
$a_{Ph}$	$m^2/m^3$	specific effective surface area of packing
$C_S$	$m/s$	$= u_V (\rho_V / (\rho_L - \rho_V))^{1/2}$ capacity factor
$D_S, d_S$	$m$	column diameter
$F_V, F_G$	$m/s (kg/m^3)^{1/2}$	$= u_V (\rho_V)^{1/2}$ gas capacity factor
$F$	-	Packing factor
$g$	$m/s^2$	$= 9.81 m/s^2$ , acceleration
$H$	$m$	section height
HETP	$m$	height equivalent to a theoretical plate
$HTU_{OV}$	$m$	overall gas side height of a transfer unit
$k_G a_{Ph}$	$1/s$	volumetric mass transfer coefficient in gas phase
$k_L a_{Ph}$	$1/s$	volumetric mass transfer coefficient in liquid phase
$L$	$kg/h$	Liquid mass flow rate
$h_L$	$m^3/m^3$	superficial liquid hold-up
$n_{th}$	-	number of theoretical stages
$p$	bar	pressure
$u_L$	$m^3/m^2h$	superficial liquid velocity
$u_V$	$m/s$	superficial gas velocity
$V, G$	$kg/h$	Vapor mass flow rate

## Greek symbols

$\beta_V a_{Ph}$	$1/s$	volumetric mass transfer coefficient in gas phase
$\beta_L a_{Ph}$	$1/s$	volumetric mass transfer coefficient in liquid phase
$\rho_L$	$kg/m^3$	liquid density
$\rho_V$	$kg/m^3$	gas density
$\Delta p/H$	$mbar/m$	specific pressure drop
$\eta$	$Pas, kg/(ms)$	dynamic viscosity

## Subscripts

FI	flooding condition
L	liquid phase
V	vapour phase

